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## NUMERICAL SIMULATION OF STRATIFIED OIL-WATER FLOW USING INTERFOAM

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### ABSTRACT

Multiphase flow of oil and water in pipes is a subject of great interest for the petroleum industry. Depending on the volumetric flow of each phase a number of different patterns can occur and, among them, the stratified flow pattern is of particular interest, because it is usually seen in horizontal pipelines. This paper presents simulations of this flow pattern using *interFoam*, a solver based on the VOF interface capturing method and available in OpenFOAM. The computational results are compared with experimental data and the predictions using an unidimensional model for global and local parameters of the flow, like pressure drop, water hold up and velocity profiles. The comparison shows good overall results for pressure drop and hold up, while the velocity profile tends to be under predicted. The CFD model is also evaluated by its capability to predict the position and shape of the fluids interface.

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**KEY WORDS:** Stratified flow, CFD, Volume-of-fluid

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### 1. INTRODUCTION

4 Many natural and industrial processes are composed of two phase flows. The stratified oil-water flow is of  
5 particular interest, because it is commonly seen in nearly horizontal pipes, like directional oil wells and  
6 pipelines.

1 A common approach to model stratified flows is the use of one dimensional methods based in Ishii and Hibiki  
 2 (1975) two-fluid equations. Using appropriate correlations, these equations can be solved for stratified liquid-  
 3 liquid flows (Brauner and Maron, 1992; Rodriguez and Baldani, 2012; Trallero, 1995) and is the most common  
 4 way to predict pressure loss and hold up for this flow pattern.

5 With the advances in computational power and parallel processing, researchers started to study the possibility  
 6 of using CFD to analyse fully three dimensional stratified flows (Berthelsen and Ytrehus, 2005; Issa, 1988;  
 7 Mouza et al., 2001; Newton and Behnia, 2001). This approach gives more detailed results using less empirical  
 8 data to its closure. The use of Volume-of-fluid (VOF), a interface capturing method, is very suited for stratified  
 9 flows and was used in a number of studies (Ghorai and Nigam, 2006; Vallée et al., 2008).

10 In this work, stratified oil-water flow is simulated using *interFoam*, the VOF solver implemented in Open-  
 11 FOAM. The results are compared with experimental data from Elseth (2001) and with the one dimensional  
 12 model of Rodriguez and Baldani (2012).

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## 2. SETUP

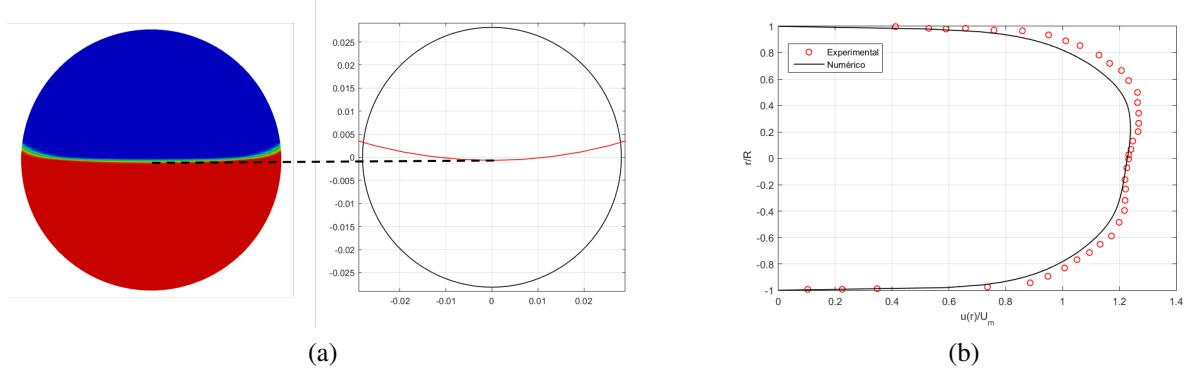
14 The flow of oil ( $\rho = 790 \text{ kg/m}^3$ ;  $\mu = 0.00164 \text{ Pa} \cdot \text{s}$ ) and water in a pipe of stainless steel of  $56.3 \text{ mm}$   
 15 of diameter is evaluated. *interFoam* solves transient RANS equations and a transport equation for the water  
 16 fraction ( $\alpha$ ). PISO method is used to couple pressure and velocity and turbulence parameters are calculated  
 17 using k- $\epsilon$  Launder-Sharma model. A structured O-H mesh is used in all the simulations, therefore a better  
 18 control of elements number, size and quality is possible.

19

## 3. RESULTS AND CONCLUSION

20 Two cases were simulated, the first for  $U_{os} = 0.34 \text{ m/s}$  and  $U_{ws} = 0.34 \text{ m/s}$  (superficial velocity of oil and  
 21 water). Figure 1 shows a good agreement between the interface shape and position for the CFD model and  
 22 the 1D model (Rodriguez and Baldani, 2012). The velocity profile is well captured, with the exception of the  
 23 regions of maximum velocity in both phases. This can be caused due to the assumption of turbulence isotropy.  
 24 Table 1 shows a good overall agreement between experiments and CFD for pressure gradient and hold up.  
 25 The 1D model was capable of providing slightly better results.

26 Figure 2 shows the same comparisons as before, for  $U_{os} = 0.3075 \text{ m/s}$  and  $U_{ws} = 0.1025 \text{ m/s}$ . Overall,  
 27 the results are good again, both for interface shape and velocity profile. Table 2 shows a bigger error between



**Fig. 1**  $U_{os} = 0.34m/s$  e  $U_{ws} = 0.34m/s$ ; (a)interface shape comparison: CFD and 1D model; (b)velocity profile comparison: CFD and experiments

**Table 1** Comparison between experiments, 1D model and CFD ( $U_{os} = 0.34m/s$  e  $U_{ws} = 0.34m/s$ )

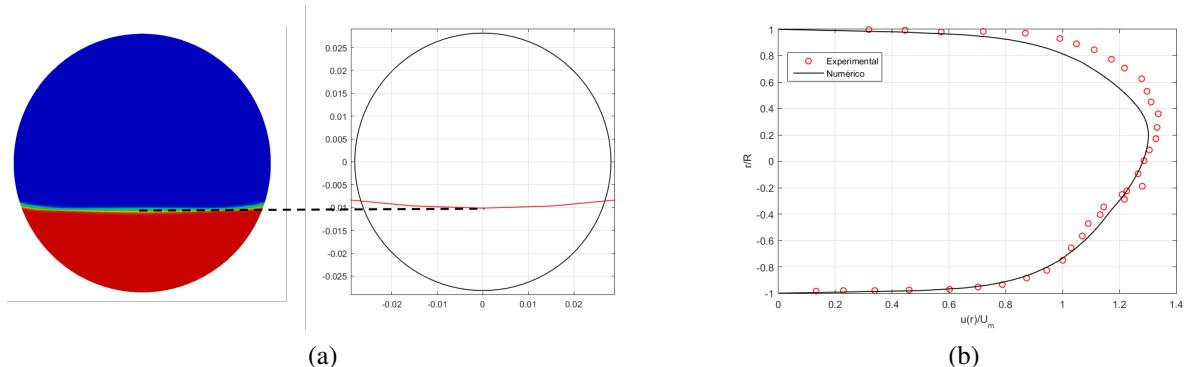
Fonte	$\partial P/\partial x$	$\epsilon_w$
Experimental	92,0 Pa/m	0,515
1D model	95,2 Pa/m	0,513
CFD model	99,4 Pa/m	0,507

1 experimental data and CFD (24.6%) for pressure gradient. A careful analysis of Elseth (2001) data indicates  
 2 that this can be caused by the presence of entrainment or an experimental error. In this case, the CFD model  
 3 shows better results than the 1D model.

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#### 4. CONCLUSIONS

5 The results show that *interFoam* is a good option to simulate stratified oil-water flows and can lead to good  
 6 predictions of pressure gradient and hold up. While the 1D model can give good results too, it depends  
 7 on correlations that have a limited range of applicability, also CFD offers detailed information of the flow



**Fig. 2**  $U_{os} = 0.3075m/s$  e  $U_{ws} = 0.1025m/s$ ; (a)interface shape comparison: CFD and 1D model; (b)velocity profile comparison: CFD and experiments

**Table 2** Comparison between experiments, 1D model and CFD ( $U_{os} = 0.3075m/s$  e  $U_{ws} = 0.1025m/s$ )

Fonte	$\partial P/\partial x$	$\epsilon_w$
Experimental	58,0 Pa/m	0, 288
1D model	38,0 Pa/m	0, 286
CFD model	43,6 Pa/m	0, 277

1 analysed. In the future, wavy stratified flow and entrainment will be investigated too.

## 2 ACKNOWLEDGMENTS

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